

## IN THE CLAIMS

1. (Currently amended) A method for withdrawing and recovering VOC and HAP emissions in the production of a lignocellulosic product, which comprises:

forming a mat of lignocellulosic material;

bonding together said mat in a product formation press with an adhesive material to produce said lignocellulosic product, wherein pressure in said formation press does not exceed about 10 psi during the formation of said lignocellulosic product, the product formation press being substantially closed to the surrounding atmosphere to contain the VOC and HAP emissions and to substantially prevent the VOC and HAP emissions from being released to the surrounding atmosphere;

forming VOC and HAP emissions during the production of said lignocellulosic product in said product formation press;

withdrawing at least about 50 % of said VOC and HAP emissions produced during the formation of said lignocellulosic product prior to removal of said lignocellulosic product from said product formation press, wherein substantially no steam is introduced into said formation press, from a source outside said formation press, during the production of said lignocellulosic product; and

recovering, without releasing to the atmosphere, said VOC and HAP emissions, which are withdrawn from said product formation press.

2. (Original) The method of claim 1, wherein said VOC and HAP emissions are continuously withdrawn from said product formation press during the formation of said lignocellulosic product.

3. (Original) The method of claim 1, wherein said VOC and HAP emissions are continuously recovered during the formation of said lignocellulosic product.

4. (Currently amended) The method of claim 1, wherein said mat is bonded together with heat and pressure substantially no steam is introduced into provided thereto by said

formation press, from a source outside said formation press, during the production of to form said lignocellulosic product.

5. (Original) The method of claim 1, wherein the step of withdrawing said VOC and HAP emissions from said product formation press during the formation of said lignocellulosic product commences no later than when said VOC and HAP emissions are formed.

Cancel claim 6.

7. (Original) The method of claim 1, wherein the VOC and HAP emissions are withdrawn from said product formation press under vacuum.

8. (Original) The method of claim 1, which further includes the step of condensing said VOC and HAP emissions, which have been withdrawn from said product formation press.

9. (Original) The method of claim 1, which includes the step of combusting said VOC and HAP emissions which have been withdrawn from said product formation press.

10. (Original) The method of claim 1, wherein said product is selected from a group consisting of particleboard and fiberboard.

11. (Original) The method of claim 1, wherein said product comprises an oriented strand board.

12. (Original) The method of claim 1, wherein said product is a multilayer product.

13. (Original) The method of claim 1, wherein the amount of air within the product formation press in the production of the lignocellulosic product is reduced by at least about 50 % of the amount of air within a product formation press employed in the production of a comparable lignocellulosic product which is produced without withdrawing said VOC and HAP

emissions from said product formation press during the production of said comparable lignocellulosic product.

14. (Original) The method of claim 1, wherein the amount of ambient air which passes through the product formation press during the formation of said lignocellulosic product is reduced by at least about 50 % of the amount of ambient air passing through the product formation press during the production of a comparable lignocellulosic product which is produced without withdrawing said VOC and HAP emissions from said product formation press during the production of said comparable lignocellulosic product.

15. (Currently amended) The method of claim 1, wherein pressure in said product formation press does not exceed about 10.5 psi during the formation of said lignocellulosic product.

16. (Original) The method of claim 1, wherein moisture content of said mat prior to the formation of said lignocellulosic product in said product formation press is more than about 6 % by weight, based on the weight said mat.

17. (Original) The method of claim 1, wherein time for decompressing and degassing said lignocellulosic product is at least about 60 % less than the time for decompressing and degassing a lignocellulosic product which is produced without withdrawing of said VOC and HAP emissions during product formation.

18. (Original) The method of claim 1, wherein the emission control system comprises at least one platen.

19. (Original) The method of claim 1, wherein the emission control system comprises a plurality of platens.

20. (Original) The method of claim 1, wherein the emission control system includes at least one screen.

21. (Currently amended) A method for recovering and controlling VOC and HAP emissions, which comprises:

forming a mat of lignocellulosic material, said mat being bonded together by an adhesive material in an emission control system to form a lignocellulosic product, said emission control system defining a product formation press for withdrawing said VOC and HAP emissions from said product formation press, wherein said pressure in said emission press system does not exceed about 50 psi during formation of said lignocellulosic product, and wherein substantially no steam is introduced into said emission press system, from a source outside said emission press system, during the production of said lignocellulosic product, said product formation press being substantially closed to the surrounding atmosphere;

forming VOC and HAP emissions during the production of said mat in said emission control system;

withdrawing said VOC and HAP emissions during the formation of said mat by evacuating said VOC and HAP emissions and controlling VOC and HAP emissions from said emission control system; and

recovering said VOC and HAP emissions which are withdrawn from said emission control system.

22. (Original) The method of claim 21, wherein said VOC and HAP emissions are continuously withdrawn from said emission control system during the formation of said lignocellulosic product.

23. (Original) The method of claim 21, wherein said VOC and HAP emissions are continuously recovered during the formation of said lignocellulosic product.

24. (Currently amended) The method of claim 21, wherein substantially no steam is introduced into said mat is bonded together by said heat and pressure which is provided from said emission press system, from a source outside said emission press system, during the production of to form said lignocellulosic product.

25. (Original) The method of claim 21, wherein the step of withdrawing said VOC and HAP emissions from said emission control system during the formation of said lignocellulosic product commences no later than when said VOC and HAP emissions are formed.

26. (Original) The method of claim 21, which further includes the step of withdrawing prior to the recovery step a substantial portion of said VOC and HAP emissions from said emission control system.

27. (Original) The method of claim 21, wherein the VOC and HAP emissions are withdrawn from said emission control system under vacuum.

28. (Original) The method of claim 21, which further includes the step of condensing said VOC and HAP emissions which have been withdrawn from said emission control system.

29. (Original) The method of claim 21, which includes the step of combusting said VOC and HAP emissions which have been withdrawn from said emission control system.

30. (Original) The method of claim 21, wherein said product is selected from a group consisting of particleboard and fiberboard.

31. (Original) The method of claim 21, wherein said product comprises an oriented strand board.

32. (Original) The method of claim 21, wherein said product is a multilayer product.

33. (Original) The method of claim 21, wherein the amount of ambient air which passes through the emission control system in the production of the lignocellulosic product is reduced by at least about 50 % of the amount of ambient air which passes through a press apparatus employed in the production of a comparable lignocellulosic product which is produced

without withdrawing said VOC and HAP emissions from said press apparatus during the production of said comparable lignocellulosic product.

34. (Original) The method of claim 21, wherein the amount of air within the product formation press during the formation of said lignocellulosic product is reduced by at least about 50 % of the amount of air within the product formation press during the production of a comparable lignocellulosic product which is produced without withdrawing said VOC and HAP emissions from said product formation press during the production of said comparable lignocellulosic product.

35. (Original) The method of claim 21, wherein pressure in said emission control system does not exceed about 10 5 psi during the formation of said lignocellulosic product.

36. (Original) The method of claim 21, wherein the moisture content prior to the formation of said lignocellulosic product in said product formation press is more than about 6 % by weight, based on the weight said mat.

37. (Original) The method of claim 21, wherein the time for decompressing and degassing said lignocellulosic product is at least about 60 % less than the cycle time for decompressing and degassing a lignocellulosic product which is produced without withdrawing of said VOC and HAP emissions during product formation.

38. (Original) The method of claim 21, wherein the emission control system comprises at least one platen.

39. (Original) The method of claim 21, wherein the emission control system comprises a plurality of platens.

40. (Original) The method of claim 21, wherein the emission control system includes at least one screen.